



## Research papers

## Evaluating the hydraulic and transport properties of peat soil using pore network modeling and X-ray micro computed tomography

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## ABSTRACT

Micro-scale properties of peat pore space and their influence on hydraulic and transport properties of peat soils have been given little attention so far. Characterizing the variation of these properties in a peat profile can increase our knowledge on the processes controlling contaminant transport through peatlands. As opposed to the common macro-scale (or bulk) representation of groundwater flow and transport processes, a pore network model (PNM) simulates flow and transport processes within individual pores. Here, a pore network modeling code capable of simulating advective and diffusive transport processes through a 3D unstructured pore network was developed; its predictive performance was evaluated by comparing its results to empirical values and to the results of computational fluid dynamics (CFD) simulations. This is the first time that peat pore networks have been extracted from X-ray micro-computed tomography ( $\mu$ CT) images of peat deposits and peat pore characteristics evaluated in a 3D approach. Water flow and solute transport were modeled in the unstructured pore networks mapped directly from  $\mu$ CT images. The modeling results were processed to determine the bulk properties of peat deposits. Results portray the commonly observed decrease in hydraulic conductivity with depth, which was attributed to the reduction of pore radius and increase in pore tortuosity. The increase in pore tortuosity with depth was associated with more decomposed peat soil and decreasing pore coordination number with depth, which extended the flow path of fluid particles. Results also revealed that hydraulic conductivity is isotropic locally, but becomes anisotropic after upscaling to core-scale; this suggests the anisotropy of peat hydraulic conductivity observed in core-scale and field-scale is due to the strong heterogeneity in the vertical dimension that is imposed by the layered structure of peat soils. Transport simulations revealed that for a given solute, the effective diffusion coefficient decreases with depth due to the corresponding increase of diffusional tortuosity. Longitudinal dispersivity of peat also was computed by analyzing advective-dominant transport simulations that showed peat dispersivity is similar to the empirical values reported in the same peat soil; it is not sensitive to soil depth and does not vary much along the soil profile.

## 1. Introduction

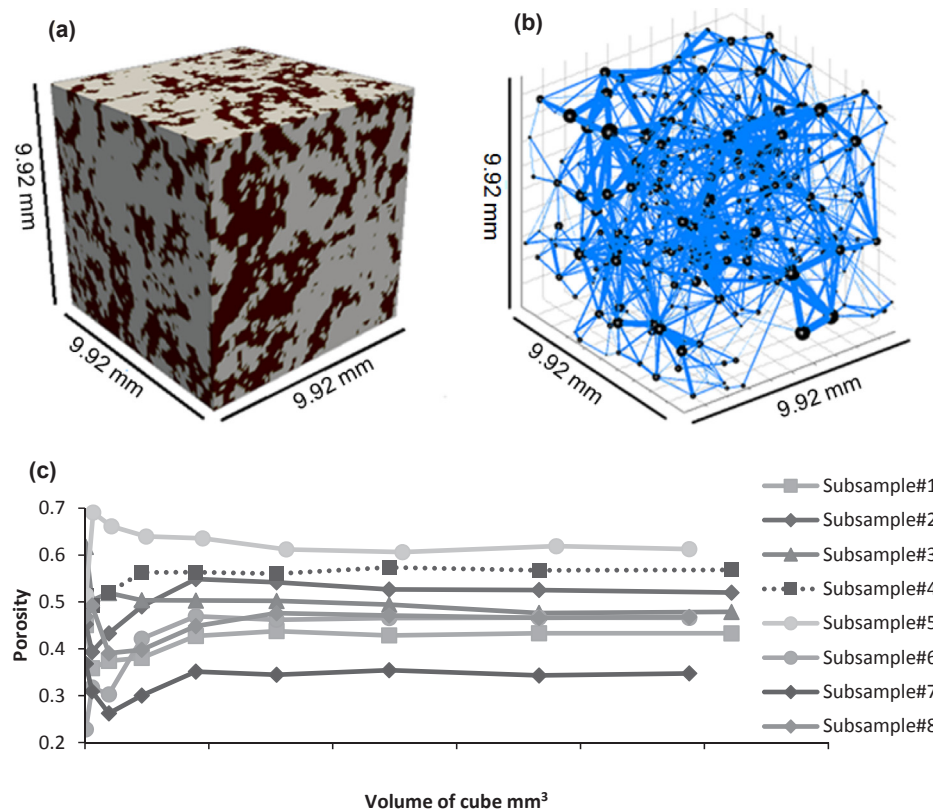
In recent years, researchers have shown an interest in studying the transport of nutrient and solutes through peatlands. Several core-scale studies (Hoag and Price, 1997; Ours et al., 1997; Quinton et al., 2008; Boudreau et al., 2009; Rezanezhad et al., 2012) and field-scale studies (Hoag and Price, 1995; Baird and Gaffney, 2000; McCarter and Price, 2017a,b) have been done to characterize the hydraulic and transport properties of peat. The properties of porous materials are controlled by micro-scale pore distribution and pore topology (Vogel, 2002). However, little attention has been paid to the link between water flow and transport properties in peat, and the role of its pore characteristics.

Quinton et al. (2008, 2009) and Rezanezhad et al. (2009, 2010) studied the relationship between peat hydraulic properties and its pore characteristics using images captured by camera or by X-ray micro computed tomography ( $\mu$ CT). These studies calculated pore conductance and pore hydraulic radius on 2D images. However, no studies have fully coupled the solute transport properties of peat soils and their relationship with micro-scale pore properties such as tortuosity and pore radius.

Pore network models (PNMs), despite having limitations, have helped to increase our understanding of multiphase flow (Vogel and Roth, 1998; Blunt, 2001; Nordhaug et al., 2003; Valvatne and Blunt, 2004; Dong and Blunt, 2009; Aghaei and Piri, 2015; Sheng and

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**Fig. 1.** (a)  $9.92 \times 9.92 \times 9.92$  mm ( $976 \text{ mm}^3$ ) X-ray  $\mu$ CT imaging data for peat soil at 2 cm depth; dark and light colors represent matrix and pore space, respectively. (b) Equivalent unstructured PNM from network extraction code; black spheres represent pore bodies (nodes) and cylinders are pore throats (bonds). (c) Examples of the variation of cube porosity versus cube volume on  $\mu$ CT images; the curves show that cube size used in this study is comparable to the REV of peat.

Thompson, 2016) and solute transport properties (Suchomel et al., 1998a; Meyers and Liapis, 1999; Bijeljic et al., 2004; Acharya et al., 2005, 2007; Bijeljic and Blunt, 2007; Raoof et al., 2013) of porous material. PNMs analyze pore morphological properties such as tortuosity (Sharratt and Mann, 1987; Armatas and Pomonis, 2004; Armatas, 2006), and can be used to characterize the relationship between pore topology and the resultant hydraulic properties of a porous media (Vogel and Roth, 2001; Arns et al., 2004). PNMs operate at a scale that can account for microscopic processes, such as the influence of a biomass accumulation and bio-clogging on permeability, in which the hydraulic properties of the medium are changing in response to flow through them (Thullner and Baveye, 2008; Ezeuko et al., 2011). Parameterizing at this scale and resolution is not practical or possible in field or even core-scale studies, especially of highly deformable *Sphagnum* dominated peat soils, while evaluating larger soil samples of peat masks the systematic reduction of peat hydraulic conductivity with depth. Therefore, PNMs provide an opportunity to better understand how peat structure, genesis, and state of decomposition affect flow and solute transport, in a detail not available through time-consuming laboratory experiments. However, it should be noted that simulation of flow and transport through 3D networks at sample sizes typical of laboratory measurements are computationally intensive.

There have been different approaches for constructing PNMs for a porous medium to represent its pore space. Previous researchers have used structured 2D (Suchomel et al., 1998b; Chen-Charpentier, 1999; Yiotis et al., 2001; Ezeuko et al., 2011) or structured 3D networks (Meyers and Liapis, 1998; Vogel, 2000; Li et al., 2006; Thullner and Baveye, 2008). A number of studies constructed PNMs using random functions obtained from  $\mu$ CT imaging data (Raoof et al., 2010; Köhne et al., 2011). Few studies extracted physically realistic disordered 3D PNMs through direct mapping the  $\mu$ CT imaging data (Al-Raoush and Willson, 2005; Silin and Patzek, 2006; Al-Kharusi and Blunt, 2007). Dong and Blunt (2009) developed a network extraction code that processes the  $\mu$ CT images to quantify the spatial distribution and geometry of pore bodies and pore throats, and their state of connectivity. They

simulated multiphase flow through the extracted pore networks and observed good agreement between simulation results and empirical data. Over decades, solute transport studies in PNMs have been studied on 3D regular networks (e.g. Acharya et al., 2005, 2007; Li et al., 2006; Raoof et al., 2010) and on irregular networks which are extracted by direct mapping of the pore space (Kim et al., 2011; Mehmani and Balhoff, 2015; Mehmani et al., 2014; Mehmani and Tchepeli, 2017). The goal of this study is to gain a better understanding of flow and transport processes in peat soils by simulating flow and transport processes through the 3D pore networks extracted through direct mapping the pore space in X-ray  $\mu$ CT images of peat deposits. The specific objectives are to (1) evaluate the characteristics of pore structure in a 3D approach for peat deposits, (2) calculate peat hydraulic properties including horizontal ( $K_h$ ) and vertical ( $K_v$ ) hydraulic conductivities and pore tortuosity ( $\tau$ ) by simulating water flow, and examine how they change with depth (hence state of peat decomposition), and (3) determine bulk solute transport properties such as hydrodynamic dispersion, longitudinal dispersivity ( $\alpha_L$ ) and effective diffusion coefficient ( $D_{eff}$ ), which are used in conventional numerical modeling, by simulating the convective/diffusive solute transport in peat pore spaces. The results help us to fundamentally answer how the variations of peat pore characteristics can influence the flow and transport properties of peat deposits. Also, since some of the parameters such as tortuosity and effective diffusion coefficient and their vertical heterogeneity along the soil profile are difficult to characterize in the laboratory, the calculated values can be used as inputs for core-scale or field-scale continuum models.

## 2. Methods and model development

Unstructured PNMs were extracted using a pore network extraction code developed by Dong and Blunt (2009). X-ray  $\mu$ CT data of *Sphagnum* peat soil at different depths (see Rezanezhad et al., 2009, 2010) were used as the input data for the network extraction code, which generated the spatial distribution and geometries of pore bodies and pore throats

including the shape, length, radius, volume and state of their interconnectivity. Fig. 1 illustrates an example of the raw 3D X-ray  $\mu$ CT data that was imported to the network extraction code (a), and the extracted PNM representing peat pore space (b). The size of voxels in the  $\mu$ CT data was 112.7  $\mu\text{m}$ , with 88 voxels along the sides of the  $\mu$ CT cubes, leading to a dimension of  $\sim 1\text{ cm}^3$  for each cube. Voxels of this size capture pores with radii  $\sim 100\text{ }\mu\text{m}$ . The majority of the interconnected macro-pores in peat, which control the bulk transport of water and solute and determine the macroscopic properties including hydraulic conductivity and dispersivity, have radii larger than  $100\text{ }\mu\text{m}$ . To explore if this sample volume adequately characterizes the peat, a representative elementary volume (REV) analysis was done on eight subsamples (Fig. 1c); it showed the cubes sufficiently exceeded the REV of porosity, thus can represent the porosity of the peat samples. However, the REV of permeability could be larger than that of porosity (Mostaghimi et al., 2013; Berg et al., 2016). Based on the work of Mostaghimi et al. (2013), the ratio of “flow-based” REV to porosity-based REV can be up to 2. Considering the cubes used here are more than twice the size of porosity REV, cubes are likely of similar dimension to the “flow-based” REV representing permeability and dispersivity. Details of the X-ray  $\mu$ CT and image processing procedures are available in Rezaeezad et al. (2009, 2010). In this study, the saturated water flow and unsteady-state solute transport processes were simulated for the extracted PNMs using the model developed herein.

The primary application of this model is to simulate saturated water flow and unsteady state solute transport through unstructured PNMs. The first module of the model simulates saturated water flow through PNMs. Water flow through a pore throat can be expressed as

$$Q_{th} = g_p \left( \frac{\Phi_{\text{Upgradient pore body}} - \Phi_{\text{Downgradient pore body}}}{l} \right) \quad (1)$$

where  $Q_{th}$  [ $\text{L}^3\text{T}^{-1}$ ] is the rate of water flow through the pore throat,  $g_p$  is pore flow conductance [ $\text{L}^5\text{TM}^{-1}$ ] calculated based on the criteria discussed in Valvatne and Blunt (2004),  $\Phi_{\text{Upgradient pore body}}$  and  $\Phi_{\text{Downgradient pore body}}$  [ $\text{ML}^{-1}\text{T}^{-2}$ ] are water pressure in the upgradient and downgradient pore bodies, respectively, and  $l$  is the pore length [ $\text{L}$ ].

The sum of water flow into a pore body equals the sum of pore throat flow rates discharging from it, giving a linear water balance equation for each pore body. Water balance equations of all pore bodies form a system of linear equations that is solved implicitly to calculate water pressure in the pore bodies (e.g. Blunt and King, 1991; Oren et al., 1998; Valvatne and Blunt, 2004). Once the pore body pressures are determined (e.g. Fig. 2), Eq. (1) is used to calculate the water flow rate in pore throats. Next, the equivalent hydraulic conductivity of the PNM is calculated using the bulk water flow rate, dimensions of the network and Darcy's law. The details on the methods used here to simulate saturated water flow in PNMs are available in Valvatne and Blunt (2004) and in (Fig. 3).

The second module of the developed code simulates advective and diffusive mass fluxes along PNMs, and calculates the concentration in pore-bodies and pore-throats during simulation. The sets of formulae for solute transport simulations are obtained from Raoof et al. (2013) and Qin and Hassanizadeh (2015); here, the formulae in those papers are reduced to the transport of a conservative tracer in the absence of chemical reactions. The final pore body and pore throat equations are Eqs. (3) and (2), respectively, which are solved iteratively (details in Fig. 3) to obtain the temporal variations of solute concentration in all the pore elements. Fig. 4 illustrates examples of solute concentration in pore bodies after a 1.5 pore volume injection, in solute transport simulations. Derivations of Eqs. (3) and (2) and definitions of their parameters are briefly included in Appendix A. Qin and Hassanizadeh (2015) provided more details on deriving and solving these equations.

$$C_{ij}^{t+\Delta t} = C_i^{t+\Delta t} \frac{(N_{ij}\max(Q_{ij},0) + N_{ij}B_{ij})}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} - C_j^{t+\Delta t} \frac{(N_{ij}\min(Q_{ij},0) - N_{ij}B_{ij})}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} + \frac{C_{ij}^t}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} \quad (2)$$

$$C_i^{t+\Delta t} \left( 1 + M_i \sum_j \max(Q_{ij},0) + M_i \sum_j B_{ij} - M_i \sum_j \frac{N_{ij}B_{ij}(|Q_{ij}| + B_{ij})}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} \right) = \left[ M_i \sum_j N_{ij} \frac{(B_{ij} - \min(Q_{ij},0))^2}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} C_j^{t+\Delta t} \right] + M_i \sum_j \frac{(B_{ij} - \min(Q_{ij},0)) C_{ij}^t}{(1 + N_{ij}|Q_{ij}| + 2N_{ij}B_{ij})} + C_i^t \quad (3)$$

The mixed cell method (MCM), which assumes a perfect mixing in pore bodies during solute transport simulation, is used here. For the media in which the mixing in the pore bodies is not perfect, MCM causes significant errors during pore network modeling of advective transport (Mehmani et al., 2014). Besides, the implementation of flow and transport equations, representation of pore space by a PNM, and numerical approximation of transport equations might introduce errors in the simulation results. Therefore, the results of the simulation code need to be evaluated against direct numerical simulation (DNS) results and empirical values. Details of the methods and the results of the evaluations are in Appendix B. The evaluation results showed a good match between DNS and PNM results. Mehmani et al. (2014) observed that the error imposed to the model's predictions due to the perfect mixing assumption is negligible in unstructured granular media. Since the pore space of peat is more unstructured than that of granular media, it is not surprising to observe similarity of DNS and PNM results, and that the assumption of perfect mixing hasn't introduced significant errors in PNM predictions. In addition, there was good agreement between PNM predictions and empirical values; all these demonstrate good predictive performance of the simulation code. It must be noted that the validity of the PNM results in this study does not justify the validity of perfect mixing in all porous media. When simulating solute transport in the PNMs of other media, DNS and PNM results must be compared to observe the quality of agreement between them and to assess the level of error imposed by simplifying assumptions of PNMs.

Nine cubes of 3D  $\mu$ CT data with dimensions of  $9.92\text{ mm} \times 9.92\text{ mm} \times 9.92\text{ mm}$  were selected from different depths of *Sphagnum* peat X-ray  $\mu$ CT data. PNM of each cube was extracted using the network extraction code of Dong and Blunt (2009). Raw simulation results, which are the spatial variations of pore body pressure and pore throat flow rates, and spatial and temporal variations of solute concentration along PNMs, were analyzed to calculate the bulk properties of peat (Fig. 3). Appendix C presents the details of the equation and algorithms used in post-processing to determine bulk properties of peat including hydraulic conductivity, effective diffusion coefficient, formation factor, hydrodynamic dispersion, longitudinal dispersivity, hydraulic tortuosity, and diffusional tortuosity. In a porous medium, hydraulic tortuosity is the ratio of actual flow length of fluid particles to the bulk length of the porous medium, and diffusional tortuosity is the ratio of actual travel length of solute species to the bulk length of the porous medium.

### 3. Results and discussion

For the peat samples used here to explore the PNM, the calculated saturated hydraulic conductivity (Table 1) was found to be high ( $\sim 2.6 \times 10^{-3}\text{ m.s}^{-1}$ ) at the near-surface layers where the poorly decomposed or living mosses cover the soil surface. Although the effective porosity declined 2.3 times, the hydraulic conductivity values declined 50 times in 10 cm of the surface peat profile, which suggests that there are reasons for the dramatic reduction of peat hydraulic conductivity



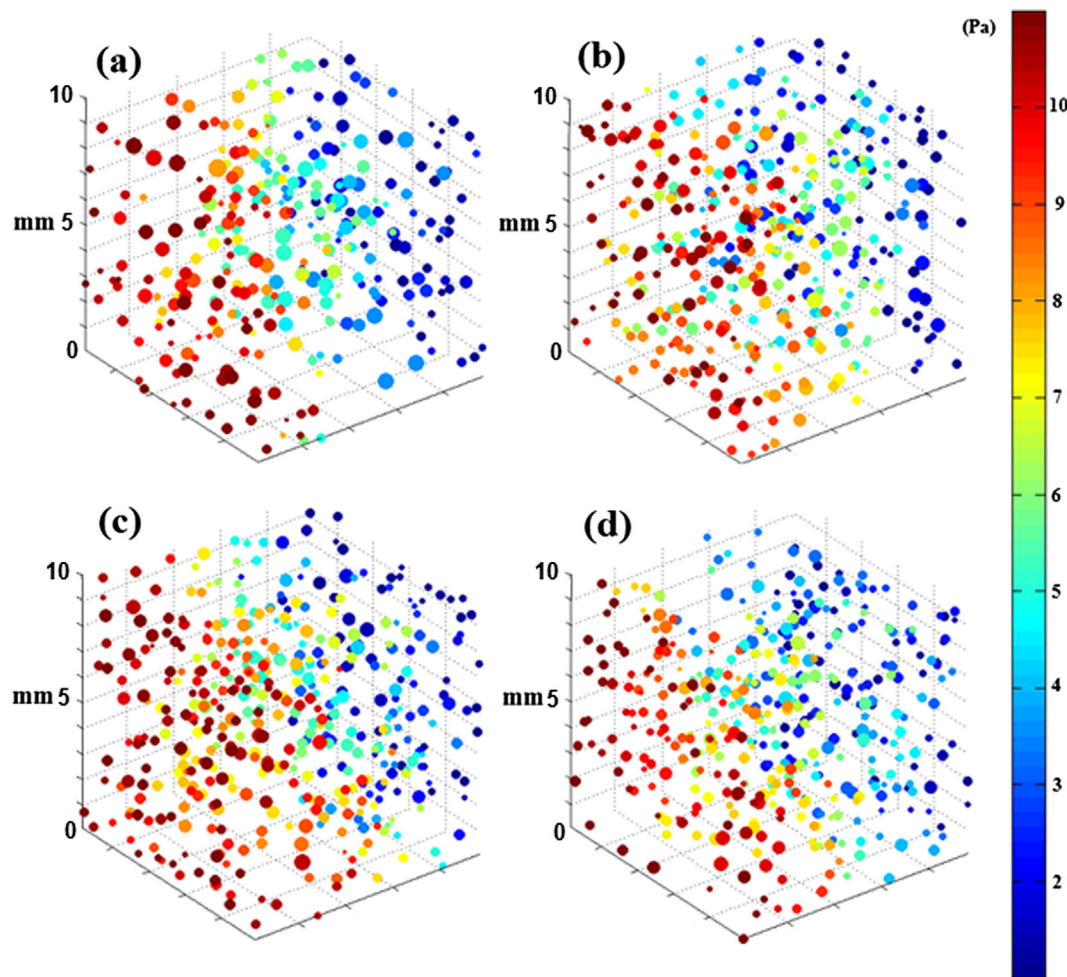


Fig. 2. Simulated pressure in pore bodies for peat soil located at (a) 2 cm, (b) 5 cm, (c) 9 cm, and (d) 10 cm depth, in which the upstream is the left face of each cube.

other than reduced effective porosity. The trend is similar to the sharp reduction of hydraulic conductivity with depth shown by Rezaeezad et al. (2010) on the same X-ray  $\mu$ CT data. A similar decline in peat hydraulic conductivity with depth has also been shown by other researchers (e.g., Boelter and Verry, 1977; Hoag and Price, 1995; Price et al., 2008).  $K_h$  at 9 cm depth was calculated to be  $6.1 \times 10^{-3} \text{ m.s}^{-1}$ ; the value is comparable to the empirical values reported by Quinton et al. (2008) for the same soil at the same depth ( $3.5 \times 10^{-3} \text{ m.s}^{-1}$  and  $1.0 \times 10^{-2} \text{ m.s}^{-1}$ ).

In this study,  $K_h$  and  $K_v$  were similar at a given depth (Table 1), illustrating isotropic hydraulic conductivity. Peat hydraulic conductivity is commonly reported to be anisotropic, with  $K_h > K_v$  (Fraser et al., 2001; Kruse et al., 2008; Lewis et al., 2012). However, anisotropy in peat can be scale-dependent, and it is not surprising to see a lack of anisotropy at small scales (Beckwith et al., 2003). Upscaling the calculated  $K_h$  values with arithmetic averaging (since horizontal flow is parallel to peat horizons), and  $K_v$  by harmonic averaging (since vertical flow is perpendicular to peat horizons) (see Bear, 1972, p.151–154) results in average  $K_h$  and average  $K_v$ , respectively, as  $1.1 \times 10^{-2}$  and  $4.5 \times 10^{-3} \text{ m.s}^{-1}$ , thus an anisotropy factor of  $\sim 2.4$  for hydraulic conductivity in the peat profile. Thus, peat hydraulic conductivity can be isotropic at the micro-scale, but due to its systematic layering, wherein  $K_h$  exceeds  $K_v$ , hydraulic conductivity becomes anisotropic at the core- or field-scale. The distinct reduction of  $K_v$  with depth in the upper peat horizons highlights an important consideration in upscaling of  $K_v$  for shallow peat layers. If we calculate  $K_v$  at a given depth, e.g. at 6 cm, the average upward  $K_v$  is the weighted harmonic mean of  $K_v$  values observed from 6 cm to 2 cm depth. Similarly, downward  $K_v$  is the

weighted harmonic mean of  $K_v$  values observed between 6 and 10 cm depth. The calculated upward up-scaled  $K_v$  and downward up-scaled  $K_v$  are  $1.34 \times 10^{-2} \text{ m.s}^{-1}$  and  $5.02 \times 10^{-3} \text{ m.s}^{-1}$  at 6 cm depth, respectively. The layered heterogeneity of peat soils and the sharply declining trend of  $K_v$  within a few centimeters lead to an apparent anisotropy of  $K_v$  that necessitates considering it in the simulation of water infiltration and solute transport through shallow peat horizons.

Decreasing peat hydraulic conductivity with depth can be due to the variations of peat pore radius with depth. The cumulative pore size distributions at 3 different depths (Fig. 5a) showed that the radii of the pores that form the pore volume of peat become smaller with increasing depth. The average pore body radius ( $R_{\text{pore, body}}$ ) and pore throat radius ( $R_{\text{pore, throat}}$ ) calculated for each PNM decreased with depth (Fig. 5b). The decrease in  $R_{\text{pore, body}}$  and  $R_{\text{pore, throat}}$  with depth explains the lower hydraulic conductivity there (Fig. 5c). The hydraulic conductivity of a porous medium is also inversely proportional to the tortuosity of the medium (Bear, 1972). To determine the hydraulic tortuosity, as shown in Fig. 3 and discussed in Appendix C, particle tracking was done on each PNM to obtain the distribution of particle's actual flow length in the network. Particle tracking results revealed that hydraulic tortuosity increases with depth (Table 1) where peat is more decomposed and has a higher bulk density (cf. Rezaeezad et al., 2010). Hydraulic tortuosity values obtained here are approximately half of the values reported by Rezaeezad et al. (2010), who estimated it as a fitting parameter, rather than directly. According to Carman (1937), increasing tortuosity reduces hydraulic conductivity. Thus, a combination of smaller pore-size and greater tortuosity with depth in a peat profile explains its lower hydraulic conductivity with depth. The average coordination number of

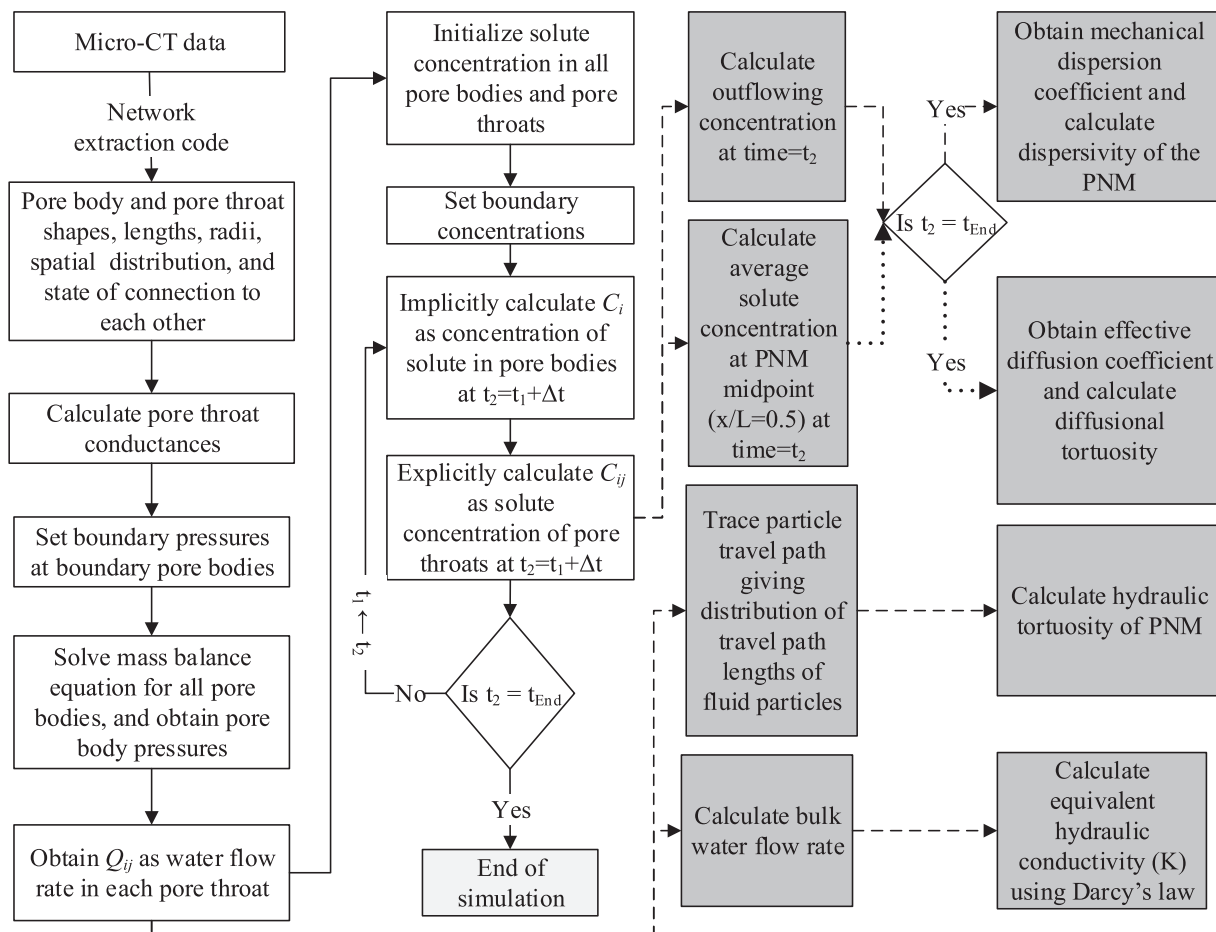


Fig. 3. Algorithm of model developed to simulate water flow and solute transport through pore networks and to calculate peat hydraulic and transport properties.

pore network, which is the average number of pore bodies that an individual pore body is connected to, decreased with increasing depth. This means that due to compaction and decomposition, the number of the connecting paths between pores decreases with depth. The reduction in average coordination number explains the increase of tortuosity with depth; as the number of pores connected to a pore body decreases, the possibility that fluid parcels travel along a straight path decreases, thus the parcel's path becomes more deviated and tortuous.

The ratio of the effective diffusion coefficient to the molecular diffusion coefficient ( $D_{eff}/D_m$ ) decreased along the depth profile (Table 1) declining from 0.38 at 2 cm depth to 0.060 at 11 cm depth. This is due to the reduction in porosity and increased tortuosity down the peat profile. Similar to hydraulic tortuosity ( $\tau_h$ ), calculated diffusional tortuosity ( $\tau_d$ ) and electrical tortuosity ( $\tau_e$ ), which is analogous to diffusional tortuosity (see Appendix C), increased with respect to peat depth (Table 1). This suggests the migration path of the diffusing solute particles becomes more tortuous with increasing degree of decomposition. For all the pore networks,  $\tau_d$  was smaller than  $\tau_h$ . This has been observed and been reported frequently for other porous material (e.g., Zhang and Knackstedt, 1995; Saomoto and Katagiri, 2015). Diffusional pore conductance is proportional to pore radius to the power of two, while hydraulic pore conductance is proportional to pore radius to the power of four; this causes flow paths of fluid particles to become more tortuous and longer than it is for solute particles (Ghanbarian et al., 2013).

The formation factor of a porous medium ( $F$ ) is a measure of the connectivity of pores in the medium based on their ability to conduct electrical current.  $F$  is determined as the ratio of the resistivity of medium when it is saturated with brine to the resistivity of the brine and is a function of porosity;  $F$  also is equal to  $D_m/D_{eff}$  (details provided

in Appendix C). Comparing  $D_m/D_{eff}$  against peat porosity (using the data of Table 1) (and fitting Eq. (C.7) from Appendix C to the data),  $a$  and  $m$ —which are parameters relating  $F$  and  $D_m/D_{eff}$  to peat porosity and are defined in Appendix C—are calculated as 0.79 and 2.41, respectively, with  $R^2$  of 0.98 (note: Quinton et al. (2008) also obtained  $m$  as 2.3 with a completely different methodology that fitted calculated hydraulic conductivity values on measured ones). It should be noted that  $m$  is a function of pore shape and specific surface area and increases as pores become irregularly shaped and as pore specific surface area rises (Salem, 2001). It also increases with increased compaction in porous material (Wyble, 1958). We know peat specific surface area increases as its average pore radius decreases with depth. Compaction of peat and the higher specific surface area in deep peat layers due to decomposition causes  $m$  to increase with depth. Larger  $m$  in deeper peat horizons leads to smaller  $D_{eff}$ , even if porosity is constant. In other words, the reduction of effective diffusion coefficient and diffusive mass flux due to increasing peat tortuosity likely is more intense in deep peat layers compared to that in near-surface horizons. This can significantly decrease the diffusion of nutrients from mineral layer beneath a peatland into the peatland. It also can prevent transport of contaminating solutes from the peat layer into the underlying mineral layer. In other word, deep highly decomposed peat layers might function as natural diffusion barriers in peatlands.

Longitudinal dispersion values were obtained by matching the simulated breakthrough curves with analytical solutions of the advection-dispersion equation, and then the longitudinal dispersion and average pore velocities were used to calculate longitudinal dispersivity (details discussed in Appendix C). Dispersivity ranged from  $2.19 \times 10^{-3}$  m to  $3.84 \times 10^{-3}$  m (Table 1). Unfortunately, few studies have reported dispersion and dispersivity values for peat, and there is a

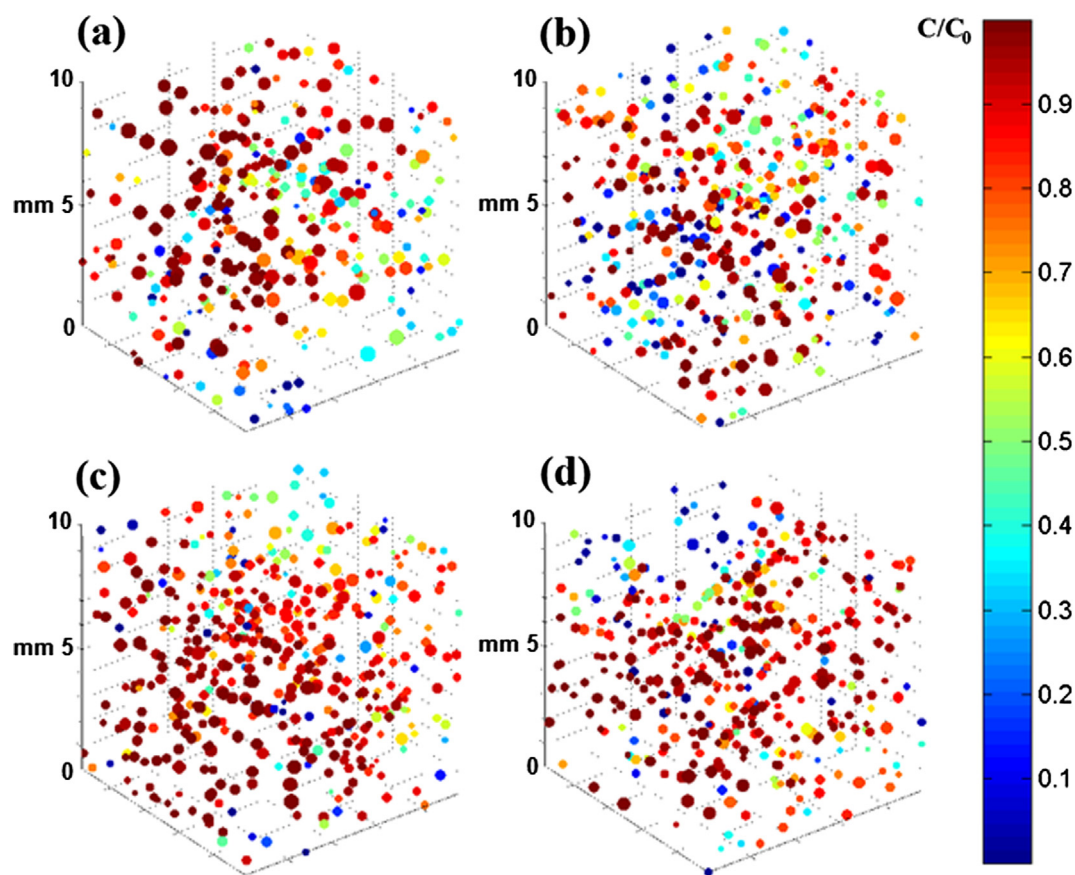


Fig. 4. Simulated solute concentration in pore bodies after 1.5 pore volume injection of solution into the pore network, obtained for peat located at (a) 2 cm, (b) 5 cm, (c) 9 cm, and (d) 10 cm depth.

gap of knowledge on how these parameters vary with peat depth and degree of decomposition. Hoag and Price (1997) measured chloride solute breakthrough curves for undisturbed peat cores obtained from a bog peatland and reported corresponding hydrodynamic dispersion values as well as average linear flow velocity. Their peat cores were extracted at 20 and 62 cm depth, and the dispersivity values were  $1.6 \times 10^{-3}$  m and  $3.72 \times 10^{-3}$  m, respectively. Our simulations resulted in similar values (Table 1). Ours et al. (1997) reported apparent dispersivity values equal to and larger than  $4.0 \times 10^{-3}$  m. However, Rosa and Larocque (2008) and Boudreau et al. (2009) reported dispersivity values an order of magnitude larger than the values obtained here. Dispersivity increases as porous media becomes more heterogeneous (Kantak et al., 1994). Klotz et al. (1980) observed that dispersivity in soil samples in laboratory tests increases as the variation of soil particle diameter increases. Increased variation of soil particle size leads to increased variations in pore radius. Variations of pore tortuosity and pore water velocity are directly related to dispersion and

dispersivity (Fetter, 1999). It is therefore likely that the notable differences between dispersivity values observed here and in Hoag and Price (1997), with the values reported by Rosa and Larocque (2008) or Boudreau et al. (2009), are due to a large variation in pore tortuosity, or pore radius in their peat samples. Further studies are required to develop a better understanding of dispersivity in peat and its relationships with the type of peat, and its depth and degree of decomposition.

#### 4. Conclusion

Simulation results with PMNs reproduced the dramatic decrease of hydraulic conductivity with respect to depth in the near-surface horizons of a peat profile that is commonly observed in field and laboratory studies (Hoag and Price, 1995, 1997; Rezanezhad et al., 2009, 2010). This is caused by a reduction of pore radius and an increase in tortuosity with depth. Diffusional tortuosity in peat, similar to other porous material, was found to be smaller than hydraulic tortuosity. Peat

Table 1

Number of pore bodies and pore throats and average pore coordination number in the extracted pore networks and the variation of active porosity ( $\epsilon_a$ ), simulated hydraulic conductivity, tortuosity ( $\tau$ ), dispersivity and  $D_{eff}/D_m$  values from 2 cm to 11 cm depth. These parameters are defined in Appendix C.

Depth (cm)	#Pore bodies	#Pore throats	Average pore coordination number	Active porosity ( $\epsilon_a$ )	$K_h$ ( $\text{m.s}^{-1}$ )	$K_v$ ( $\text{m.s}^{-1}$ )	Hydraulic tortuosity $\tau_h$	$D_{eff}/D_m$	Electrical and diffusional tortuosity $\tau_e, \tau_d$	Longitudinal dispersivity ( $\alpha_L$ ) (m)
2	311	1398	9.0	0.61	$2.63 \times 10^{-2}$	$2.50 \times 10^{-2}$	2.05	0.38	1.27	$2.86 \times 10^{-3}$
3	312	1329	8.5	0.57	$2.33 \times 10^{-2}$	$2.23 \times 10^{-2}$	1.87	0.35	1.28	$3.69 \times 10^{-3}$
5	490	1590	6.5	0.47	$8.14 \times 10^{-3}$	$9.00 \times 10^{-3}$	2.07	0.21	1.48	$3.84 \times 10^{-3}$
6	406	1658	8.2	0.49	$1.05 \times 10^{-2}$	$1.14 \times 10^{-2}$	1.96	0.24	1.44	$3.12 \times 10^{-3}$
9	452	1780	7.9	0.47	$6.10 \times 10^{-3}$	$5.80 \times 10^{-3}$	2.19	0.19	1.59	$2.19 \times 10^{-3}$
10	433	1357	6.3	0.35	$1.59 \times 10^{-3}$	$1.56 \times 10^{-3}$	2.3	0.086	2	$2.29 \times 10^{-3}$
11	469	1302	5.6	0.27	$4.56 \times 10^{-4}$	$4.52 \times 10^{-4}$	2.48	0.06	2.12	–

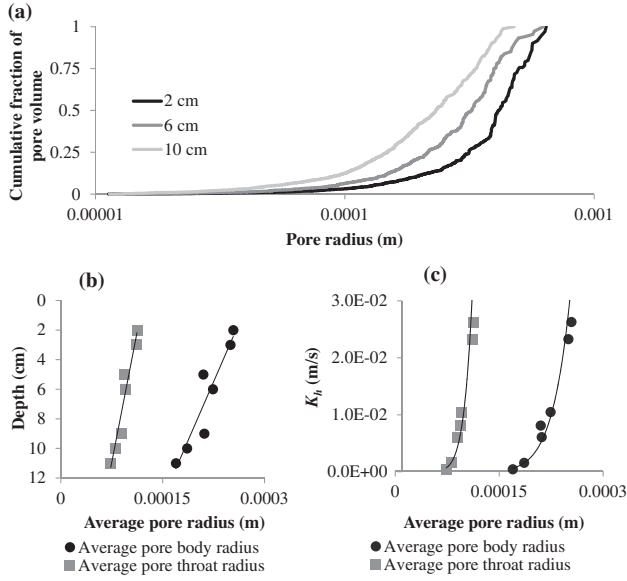


Fig. 5. (a) cumulative distributions of pore radii in different peat depths. (b) variation of peat average pore radius with depth. (c) variation of peat horizontal hydraulic conductivity with average pore radius.

dispersivity was determined through advection dominant transport PNM simulations, which showed that peat dispersivity does not vary considerably with depth. The values are in the same range of observed

values for similar type of peat at similar depths (Hoag and Price, 1997; Ours et al. (1997)). This study confirms that hydraulic properties of peat soils are controlled by their pore size and pore tortuosity.

Characterizing the effective diffusion coefficient of a porous medium by laboratory experiments is a time consuming process fraught with practical/technical difficulties, and conventional modeling of diffusion-dominant transport through peat soils requires an estimate of the effective diffusion coefficient. The PNM resulted the effective diffusion coefficient and its variation with depth through simulation of non-advective solute transport, illustrating that due to increasing tortuosity its decrease relative to pure molecular diffusion with depth. The effective diffusion coefficient of peat and its variation with depth received little attention in previous studies. Results suggested that the reduction in effective diffusion can be more intense in deeper peat horizons with higher states of decomposition.

Because of limitations in computational capabilities, network modeling is currently unable to simulate meso-scale or field-scale transport processes. However, based on small samples it can be used to extend fundamental knowledge on pore-scale phenomena, and to address how peat pore morphology controls the larger scale properties of peat. Furthermore, it can be used to characterize the systematic heterogeneities of pore morphology that cannot be physically measured.

#### Acknowledgements

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#### Appendix A. Derivation of solute transport equations

The code solves the solute mass balance equations for the pore elements

$$V \frac{dC}{dt} = (QC)_{in} - (QC)_{out} - \left( D_m A \frac{dC}{dl_p} \right)_{in} + \left( D_m A \frac{dC}{dl_p} \right)_{out} \quad (A.1)$$

where  $V$  is the volume of a pore element (pore body or pore throat) [ $L^3$ ],  $Q$  is the rate of water flowing into or out of the pore element [ $L^3 T^{-1}$ ],  $C$  is the solute concentration at the pore element [ $ML^{-3}$ ],  $D_m$  is the molecular diffusion coefficient of solute [ $L^2 T^{-1}$ ],  $l_p$  is the length of pore element [ $L$ ], and  $dC/dl_p$  is the concentration gradient along the pore element [ $ML^{-4}$ ] which later is approximated as the gradient between a pore body (pore throat) and its adjacent pore throat (pore body). Applying Eq. (A.1) for pore throats and pore bodies (with considering multiple inlets/outlets in the pore bodies), Eqs. (2) and (A.3) are obtained for pore bodies and pore throats respectively, where  $i$  and  $j$  are the pore body indexes, and  $ij$  is the index of the pore throat that is connecting pore body  $i$  to pore body  $j$ .

$$V_i \frac{dC_i}{dt} = -C_i \sum_j \max(Q_{ij}, 0) - \sum_j C_{ij} \min(Q_{ij}, 0) - \sum_j D_{ij} A_{ij} \frac{C_i - C_{ij}}{L_{ij}/2} \quad (A.2)$$

$$V_{ij} \frac{dC_{ij}}{dt} = (C_i - C_{ij}) \max(Q_{ij}, 0) + (C_{ij} - C_j) \min(Q_{ij}, 0) + D_{ij} A_{ij} \frac{(C_i - C_{ij})}{\left(\frac{L_{ij}}{2}\right)} + D_{ij} A_{ij} \frac{(C_j - C_{ij})}{\left(\frac{L_{ij}}{2}\right)} \quad (A.3)$$

Using an upwind scheme in approximating Eq. (A.2), Eq. (A.4), which is the numerically approximated form of solute transport equation in pore bodies, is obtained;  $M_i$  and  $B_{ij}$  are defined in Eqs. (A.5) and (A.6) respectively.

$$C_i^{t+\Delta t} = -M_i C_i^{t+\Delta t} \sum_j \max(Q_{ij}, 0) - M_i \sum_j C_{ij}^{t+\Delta t} \min(Q_{ij}, 0) - M_i \sum_j B_{ij} (C_i^{t+\Delta t} - C_{ij}^{t+\Delta t}) + C_i^t \quad (A.4)$$

$$M_i = \frac{\Delta t}{V_i} \quad (A.5)$$

$$B_{ij} = \frac{2D_{ij}A_{ij}}{L_{ij}} \quad (A.6)$$

Numerically approximating the Eq. (A.3) with upwind scheme and rearranging the obtained equation leads to Eq. (2), which is the final form of solute transport equation in pore throats; as defined in Eq. (A.7),  $N_{ij}$  is the ratio of time step size to the pore throat volume.

$$C_{ij}^{t+\Delta t} = C_i^{t+\Delta t} \frac{(N_{ij} \max(Q_{ij}, 0) + N_{ij} B_{ij})}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} - C_j^{t+\Delta t} \frac{(N_{ij} \min(Q_{ij}, 0) - N_{ij} B_{ij})}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} + \frac{C_j^t}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} \quad (2)$$



$$N_{ij} = \frac{\Delta t}{V_{ij}} \quad (\text{A.7})$$

Finally Eq. (3) is obtained by coupling Eqs. (2) and (A.4). Eqs. (2) and (3) are solved iteratively to calculate the temporal variations of solute concentrations in pore elements. The details of equations derivations and numerical solution procedure are presented in Qin and Hassanizadeh (2015).

$$C_i^{t+\Delta t} \left( 1 + M_i \sum_j \max(Q_{ij}, 0) + M_i \sum_j B_{ij} - M_i \sum_j \frac{N_{ij} B_{ij} (|Q_{ij}| + B_{ij})}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} \right) = \left[ M_i \sum_j N_{ij} \frac{(B_{ij} - \min(Q_{ij}, 0))^2}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} C_j^{t+\Delta t} \right] + M_i \sum_j \frac{(B_{ij} - \min(Q_{ij}, 0)) C_j^t}{(1 + N_{ij} |Q_{ij}| + 2N_{ij} B_{ij})} + C_i^t \quad (3)$$

## Appendix B. Model evaluation

Flow and solute transport must first be validated by ensuring water and solute mass conservation. Water mass conservation in saturated flow simulations requires that the bulk rate of water flowing into the PNM equals the bulk rate of water flowing out. This is validated in the pore network simulation when the difference between the inflow and outflow rate is negligible (less than 0.001%). The conservation of solute mass in solute transport simulations needs

$$M_{\text{injected}}(t) = M_{\text{produced}}(t) + M_{\text{accumulated}} \quad (\text{B.1})$$

where  $M_{\text{injected}}$  is cumulative injected solute mass [M],  $M_{\text{produced}}$  is cumulative produced (outflow) solute mass [M], and  $M_{\text{accumulated}}$  is the mass of solute accumulated in the aqueous phase present in the pore network [M].  $M_{\text{injected}}$ ,  $M_{\text{produced}}$ ,  $M_{\text{accumulated}}$  were calculated as

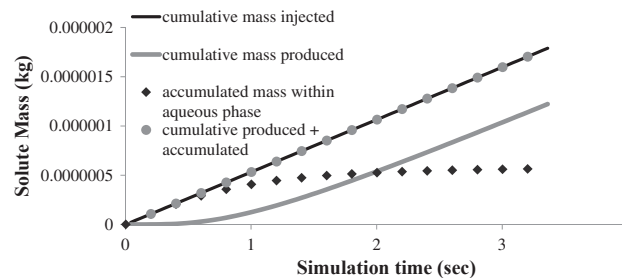
$$M_{\text{injected}}(t) = Q_w \int_{t=0}^t C_0 dt = C_0 Q_w t \quad (\text{B.2})$$

$$M_{\text{produced}}(t) = Q_w \int_{t=0}^t C_{\text{outflow}} dt \quad (\text{B.3})$$

$$M_{\text{accumulated}}(t) = \sum_{i=1}^{N_{\text{pore body}}} C_i(t) V_i + \sum_{j=1}^{N_{\text{pore throat}}} C_j(t) V_j \quad (\text{B.4})$$

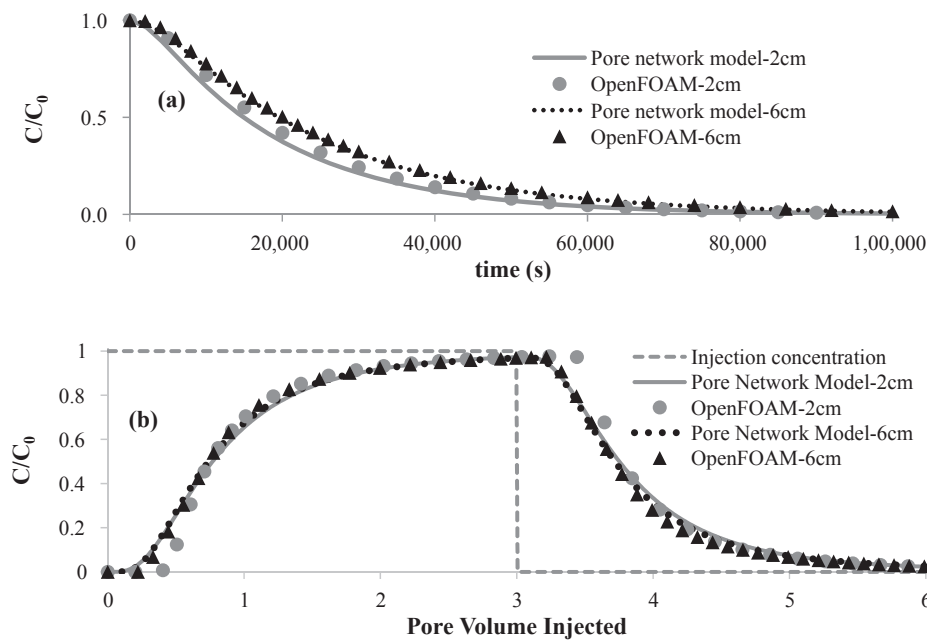
where  $C_0$  [ $\text{ML}^{-3}$ ] is the source concentration,  $Q_w$  is the bulk water flow rate [ $\text{L}^3 \text{T}^{-1}$ ], and  $t$  is simulation time [T],  $C_{\text{outflow}}$  [ $\text{ML}^{-3}$ ] is the solute concentration at the outflow face of the pore network,  $C_i(t)$  is solute concentration at pore body  $i$  at time  $t$ ,  $C_j(t)$  is solute concentration at pore throat  $j$  at time  $t$ ,  $V_i$  is the volume of pore body  $i$ ,  $V_j$  is the volume of pore throat  $j$ ,  $N_{\text{pore body}}$  is number of pore bodies in the pore network, and  $N_{\text{pore throat}}$  is the number of pore throats in the pore network. Fig. B.1 illustrates an example of the aforementioned parameters in a solute transport simulation showing that Eq. (B.1) and consequently solute mass conservation are valid in the transport simulations.

The second step in validating the pore network modeling code was to compare its results to the results of direct numerical simulations (DNS) done using OpenFOAM, which is an open-source computational fluid dynamics (CFD) tool. An OpenFOAM model was constructed for each depth from the same X-ray  $\mu\text{CT}$  cube used for pore network extraction. First, the STereoLithography (STL) file of the surface representing the outer boundaries of the pore space in  $\mu\text{CT}$  images was exported using MICROVIEW (version 2.5.0-rc12). Next, a 3D mesh of the void space was constructed using blockMesh and snappyHexMesh, the meshing tools of OpenFOAM. Then, water flow and solute transport processes were simulated on the 3D mesh with boundary conditions and initial conditions identical to those used in the pore network simulations. For advective dominant simulations, the following steps are done: (1) A pressure gradient similar to that of pore network model is applied along the 3D mesh, and the Navier-Stokes equation is solved using icoFOAM solver of OpenFOAM, resulting in pressure and velocity variations along the 3D mesh; and (2) the simulated velocity vector is inserted as boundary condition and initial condition in transport simulations in which the initial concentration of solute in the 3D mesh is zero, the inflow boundary condition is a pulse injection of solute with a concentration of  $C = C_0$  for half the simulation time and then  $C = 0$  for the rest of simulation time (Fig. B.2); the outflow boundary condition is zero gradient. ScalarTransportFoam solver of OpenFOAM package is used to simulate concentration variations over time and space. For the diffusional cases, the elements of the velocity vector is considered zero (no advection) along the 3D mesh; initial solute concentration is  $C = C_0$  along the 3D mesh, and boundary conditions at two end faces of the domain are  $C = 0$ . Eventually, post-processing of the simulation results, which are the variation of solute concentration in the 3D mesh with time, was done using



**Fig. B.1.** Example of solute mass balance in peat pore network solute transport simulations for the PNM at 2 cm depth; black line shows the variation of  $M_{\text{injected}}$  with simulation time, grey line illustrates the variation of  $M_{\text{produced}}$  over simulation time, black diamonds are  $M_{\text{accumulated}}$  in the pore network over simulation time, and grey circles represent the sum of  $M_{\text{accumulated}}$  and  $M_{\text{produced}}$ , which strongly matches the cumulative mass injected (black line), meaning that the solute mass balance error is negligible and solute mass conservation is valid along the simulation time.



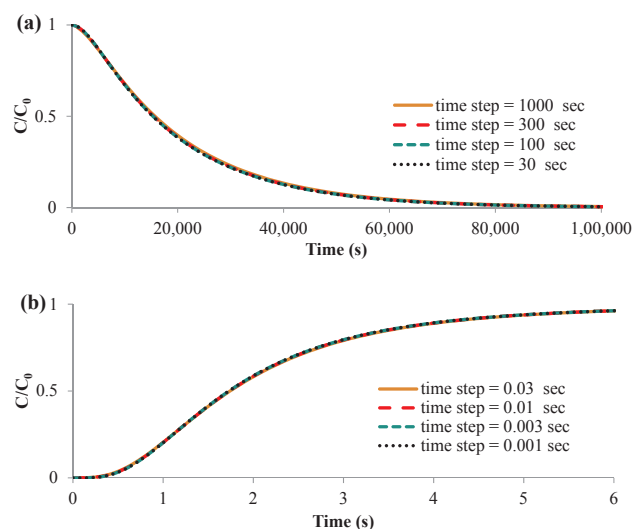


**Fig. B.2.** (a) Variation of solute concentration at  $x = L/2$  of peat pore space in a diffusional transport process for peat at 2 and 6 cm depth, (b) variation of effluent solute concentration in an advective-dominant transport process, obtained by direct simulations with OpenFOAM, and by developed pore network modeling code for peat at 2 and 6 cm depth.

processing functions of PARAVIEW (Ahrens et al., 2005; Ayachit, 2015). In both diffusional transport simulations (Fig. B.2a) and advection-dominant transport simulations (Fig. B.2b), PNM results are in good agreement with DNS results. For sample of 6 cm depth, the matching quality in the declining part of the breakthrough curve (BTC) remained as good as the concentration rise part. For peat of 2 cm depth, mismatches are seen at the beginning of the rise and at the decline portion of the BTC; however, in the mid-concentrations and at the tails of the BTC matching quality is good. This early breakthrough might be due to a slight misrepresentation of the pore space by the network model; in direct mapping the pore space, a portion of the active pore volume might be assigned to pores bodies or pore throats that are not as actively transporting water (e.g. dead-end pores). Therefore, due to the underestimation of the active pore volume, which is transferring the advective flux, solute's arrival time is underestimated and the earlier breakthrough takes place at the outflow (Mehmani and Tchelepi, 2017). As the simulation time proceeds, the less-active pores contribute to the solute transport through diffusion which returns the BTC of PNM to the trend of the BTC of DNS.

The agreements between PNM and DNS results means the implementation of flow and transport equations in the pore network modeling code discussed in Section 2 and Appendix A has been done successfully. In addition, it shows the numerical approximation of the flow and transport equations, the approximation of pore spaces with the networks of pore bodies and pore throats, and the assumption of perfect mixing in the pore bodies impose little error on the predictions of PNM. The successful verification of the developed code allows us conducting forward simulations and predicting the hydraulic and transport properties of PNMs.

The third step in evaluating the pore network modeling result was to determine the sensitivity of the results to the size of time step and the effects of numerical diffusion on the simulation results. The sensitivity of simulation results to the size of time step was studied for diffusional transport and advection-dominant transport cases on the pore network of 2 cm depth peat (Fig. B.3). The figure shows that simulation results are very similar in the runs with different time steps, which means that the results are independent of the sizes of time steps. Numerical diffusion is a matter of concern in the numerical simulation of transport processes and its significance depends on the size of time step. Since in a given PNM simulation study, the



**Fig. B.3.** (a) variation of solute concentration at  $x = L/2$  of peat pore space in a diffusional transport process for peat of 2 cm depth at different time step sizes, (b) variations of effluent solute concentration in an advective-dominant transport process for peat of 2 cm depth at different time step sizes.

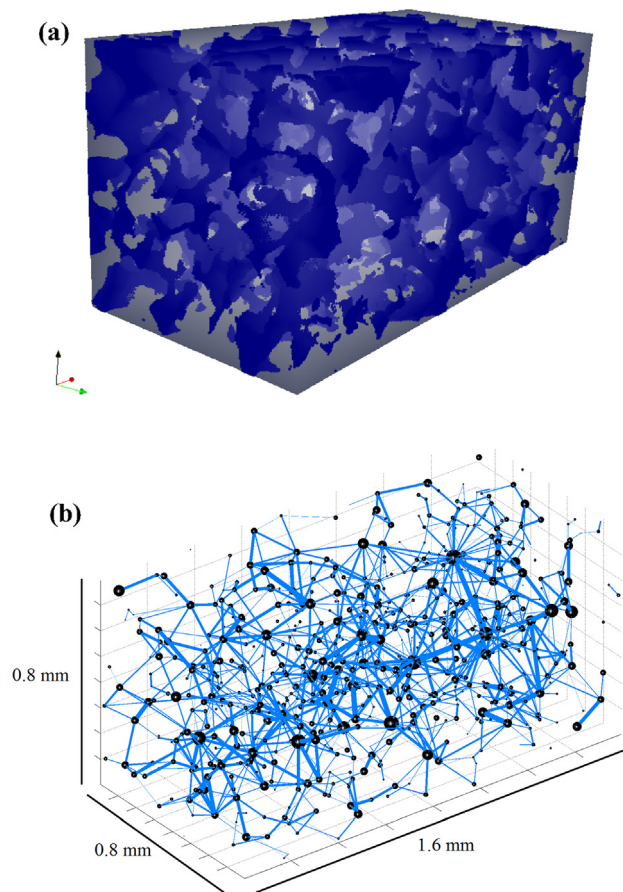


Fig. B.4. (a) CT scan imaging data of Berea sandstone (Imperial College) for sample #1, and (b) the extracted pore network.

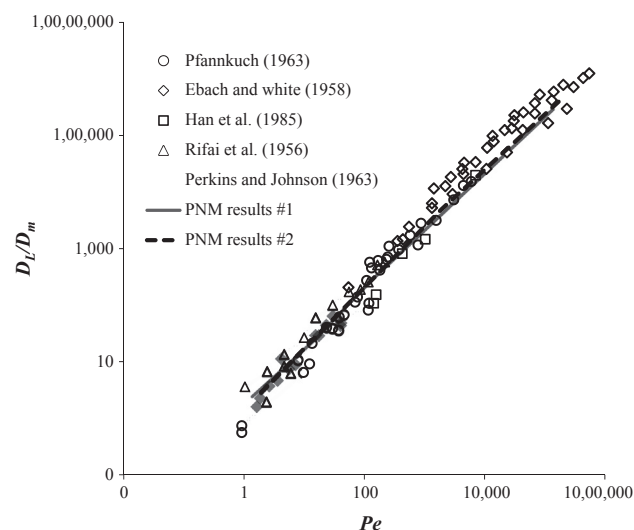


Fig. B.5. Measured  $D_L/D_m$  versus Peclet number for granular porous media in comparison to simulated values for Berea sandstone. (See above-mentioned references for further information.)

results do not vary with the size of simulation time step (Fig. B.3) it can be assumed that time step sizes were adequately small to keep the effect of numerical diffusion insignificant compared to the effect of physical transport processes.

The fourth step in validating the pore network modeling code was to compare its results obtained for Berea sandstone to the empirical data available in literature. Bijeljic et al. (2004) constructed PNM using pore data of Berea sandstone, and modeled solute transport at the pore-scale. They compared the calculated  $D_L/D_m$  vs. Peclet number ( $Pe$ ) to the empirical data that were measured for granular porous material and obtained a good agreement between them. A similar evaluation was done in this study. Two subsections ( $802 \mu\text{m} \times 802 \mu\text{m} \times 1604 \mu\text{m}$ ) were cut from micro-CT image of Berea sandstone (available in Imperial-College website with resolution of  $5.345 \mu\text{m}$ ) (subsection#1 in Fig. B.4a), and the pore network of each was extracted (Fig. B.4b for subsection#1). Then advective-diffusive transport was simulated along each network at different pore water

velocities, and the dispersion coefficient in each simulation was determined by methodology discussed in Appendix C. The calculated  $D_L/D_m$  to  $Pe$  relations are compared to the empirical data (Fig. B.5). In Fig. B.5, symbols are empirical data of granular media and – excluding Perkins and Johnson (1963) – are reproduced from Han et al. (1985). The grey line and black dashed line are the results of our model, respectively, for subsections #1 and #2. There is a good agreement between our results and the empirical data confirming that our simulation code has a good predictive performance.

### Appendix C. Evaluation of bulk hydraulic and transport properties

#### Hydraulic conductivity

As the simulation of saturated water flow in a pore network ends,  $Q_w$ , which is the bulk water flow rate through the pore network [ $L^3T^{-1}$ ], is calculated using the flow rate of each pore throat (Fig. 3). Using dimensions of pore network and applied upstream and downstream pressures, the equivalent permeability of the pore network is calculated using a form of Darcy's law, given as

$$k_{eq} = \frac{Q_w \mu_w L}{A_{bulk} (P_{upstream} - P_{downstream})} \quad (C.1)$$

where  $k_{eq}$  is the equivalent permeability of pore network [ $L^2$ ],  $Q_w$  is bulk water flowing rate [ $L^3T^{-1}$ ],  $\mu_w$  is water viscosity [ $MT^{-1}L^{-1}$ ],  $L$  is the bulk length of the cube [ $L$ ],  $A_{bulk}$  is bulk cross-sectional area of the soil cube [ $L^2$ ], and  $P_{upstream}$  and  $P_{downstream}$  are water pressures [ $ML^{-1}T^{-2}$ ] at the upstream and downstream faces of the network, respectively. The equivalent hydraulic conductivity of the pore network is then calculated by

$$K_{eq} = \frac{k_{eq} \rho_w g}{\mu_w} \quad (C.2)$$

where  $K_{eq}$  is equivalent hydraulic conductivity [ $LT^{-1}$ ],  $\rho_w$  is water density [ $ML^{-3}$ ], and  $g$  is acceleration by gravity [ $LT^{-2}$ ] (Freeze and Cherry, 1979). Horizontal hydraulic conductivity ( $K_h$ ) and vertical hydraulic conductivity ( $K_v$ ) of each PNM were determined by applying pressure gradients in the horizontal (e.g. Fig. 2) and vertical directions, respectively.

#### Hydraulic tortuosity

Depending on the type of traveling particles, the hydraulic tortuosity ( $\tau_h$ ) and diffusional tortuosity ( $\tau_d$ ) are defined for porous media (Clennell, 1997). When fluid particles move through a porous medium the path is tortuous due to the presence of solids, which form flow and transport barriers. The extension of fluid particle movement path necessitates definition of  $\tau_h$  as

$$\tau_h = \frac{L_{actual}}{L_{apparent}} \quad (C.3)$$

where  $L_{actual}$  is the average length of the path that a fluid particle moves through the pore space, and  $L_{apparent}$  is the bulk length of porous medium (Bo-Ming and Jian-Hua, 2004; Shen and Chen, 2007).

We obtained the  $\tau_h$  of peat by tracking fluid particles through PNMs. A number of fluid particles ( $N = 10^4$ ) were placed at the upstream face of the pore network, and the flow path of each particle is tracked until the particle arrives at the downstream face of the network. The average travel path length is calculated as arithmetic mean of the travel length of all the particles.  $\tau_h$  of pore network is then calculated as the ratio of the average travel length to the bulk length of the network (Fig. C.1).

#### Diffusional tortuosity and pore shape exponent

Similar to fluids particles, when solute particles move by a diffusional transport, the presence of solids causes the actual path to be longer than bulk length of the porous media. The longer solute travel path in the presence of soil solids reduces the diffusive mass flux and causes the bulk effective diffusion coefficient ( $D_{eff}$ ) [ $L^2T^{-1}$ ] to be smaller than the molecular diffusion coefficient ( $D_m$ ) [ $L^2T^{-1}$ ] for that solute in water. The relation

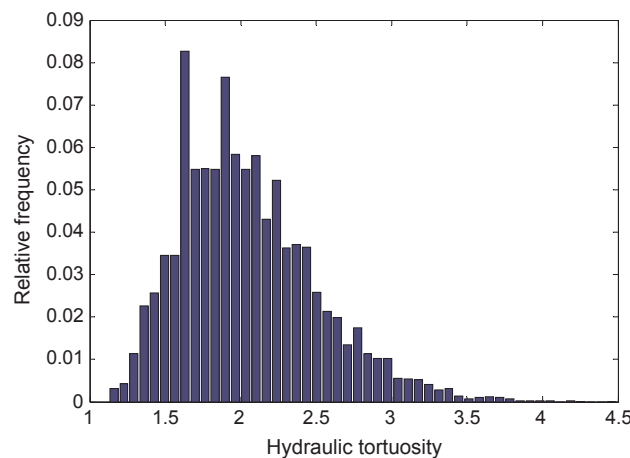


Fig. C.1. Histogram of hydraulic tortuosity of peat PNM at 2 cm depth; the average tortuosity is 2.05 as indicated in Table 1.

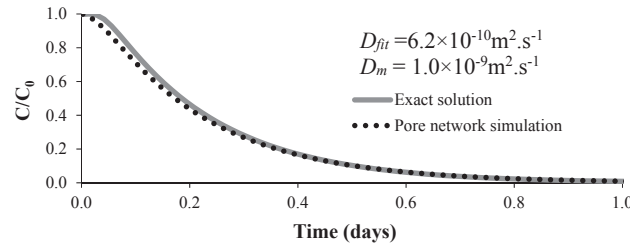


Fig. C.2. Comparison of analytical solution and pore network modeling solution for variation of solute concentration at  $x = L/2$  of a peat cube at 2 cm depth.

between ratios of  $D_{eff}$ ,  $D_m$ ,  $\tau_d$ , and  $\varepsilon$  of porous media (Moldrup et al., 2001; Gommès et al., 2009) is

$$\tau_d^2 = \frac{D_m \varepsilon}{D_{eff}} \quad (C.4)$$

To calculate  $D_{eff}$  of pore networks by network simulations, the water flow rate is assumed to be zero, so the transport process is non-advective. A well-known diffusional transport problem having an exact analytical solution is a cube with length  $L$  [L], initial solute concentration of  $C_0$  [ML<sup>-3</sup>], and boundary conditions of  $C(0,t) = C(L,t) = 0$ . The exact solution for the variation of solute concentration over time and space in the cube is

$$C(x,t) = \frac{4C_0}{\pi} \sum_{i=1}^{\infty} \left[ \frac{1}{2i-1} \sin\left(\frac{(2i-1)\pi x}{L}\right) \exp\left(-\frac{(2i-1)^2 \pi^2 D_{fit} t}{L^2}\right) \right] \quad (C.5)$$

where  $x$  is position of observation point [L],  $D_{fit}$  is the equivalent diffusion coefficient [L<sup>2</sup>T<sup>-1</sup>] of the system, and  $t$  is time [T] (Mehrer, 2007). Non-advective solute transport through PNMs is simulated with the same initial condition and the same boundary conditions of the abovementioned problem. To obtain  $D_{fit}$  of a pore network, the temporal variation of solute concentration at  $x/L = 0.5$  that results from the pore network simulation is compared to that resulting from Eq. (C.5) at  $x = L/2$ . Then  $D_{fit}$  in Eq. (C.5) is adjusted until the solute concentration variation at  $x = L/2$  fits the pore network simulation results and the sum of the square of the errors minimizes. Fig. C.2 illustrates an example of pore network simulation results and the fitted exact solution for a peat cube at 2 cm depth. The calculated  $D_{fit}$  ( $5.9 \times 10^{-10} \text{ m}^2 \cdot \text{s}^{-1}$  in Fig. C.2) is around half of  $D_m$  ( $1.0 \times 10^{-9} \text{ m}^2 \cdot \text{s}^{-1}$ ) because of the  $\tau_d$  of peat. Since  $D_{fit}$  is back-calculated from the concentration of the solution, it is the effective diffusion coefficient in the aqueous phase. Therefore,  $D_{eff}$ , which is the bulk effective diffusion coefficient, is the product of  $D_{fit}$  and the porosity. Eventually, diffusional tortuosity,  $\tau_d$ , can also be calculated using Eq. (C.4) and the calculated  $D_{eff}$ .

The formation factor ( $F$ ) of a porous medium, which is the ratio of electrical conductivity of pure brine to the electrical conductivity of the medium when it is saturated with brine, is inversely correlated with porosity of the porous material by

$$F = \frac{a}{\varepsilon^m} \quad (C.6)$$

where  $a$  is a parameter affected by tortuosity,  $\varepsilon$  is the porosity, and  $m$  is the shape (cementation) exponent (Archie, 1942; Winsauer et al., 1952; Liu and Kitanidis, 2013). In this equation, both  $a$  and  $m$  are empirical parameters and are controlled by pore shape and geometry (Boving and Grathwohl, 2001), and  $a$  is different from classic tortuosity (Salem, 1993). Due to the analogy between Ohm's Law as the electrical charge transport equation and Fick's law as the solute transport equation (Klinkenberg, 1951; Liu and Kitanidis, 2013), and considering electrical and diffusional tortuosity ( $\tau_d$ ) are the same (Sahimi, 1994; Clennell, 1997), the formation factor ( $F$ ) is equal to the ratio of  $D_m$  to  $D_{eff}$  (Snyder, 2001). Therefore

$$\frac{D_m}{D_{eff}} = a\varepsilon^{-m} \quad (C.7)$$

As corresponding  $\varepsilon$  of all the PNMs and  $D_m$  of the solute are known in solute transport simulations, Eq. (C.7) suggests  $m$  and  $a$  can be calculated by obtaining  $D_{eff}$  of at least two pore networks. After fitting  $D_{fit}$  and calculating  $D_{eff}$  for the pore networks,  $\tau_d$  of each network as well as  $a$  and  $m$  are calculated using Eqs. (C.4) and (C.7).

### Dispersivity

Dispersivity is a transport parameter controlling the mixing length between streams of the aqueous phase, such that

$$D_L = \alpha_L v + D_{eff} \quad (C.8)$$

where  $\alpha_L$  is longitudinal dispersivity [L],  $v$  is average linear flow velocity [LT<sup>-1</sup>],  $D_{eff}$  is effective diffusion coefficient [L<sup>2</sup>T<sup>-1</sup>], and  $D_L$  is hydrodynamic dispersion [L<sup>2</sup>T<sup>-1</sup>] (Appelo and Postma, 2004). Based on this equation, if a set of  $D_L$  vs.  $v$  data points are available for a porous medium, dispersivity of the medium is calculated as the slope of linear regression. The average linear flow velocity in a porous medium is determined (Appelo and Postma, 2004) as

$$v = \frac{Q_w}{A_{bulk} \varepsilon} \quad (C.9)$$

Hydrodynamic dispersion ( $D_L$ ) and longitudinal dispersivity ( $\alpha_L$ ) for an advective-diffusive transport process is obtained by analyzing the simulated solute breakthrough curves. In the simulation of unsteady-state solute transport through PNMs, the variation of effluent concentrations with time is the solute breakthrough curve. We fit the simulated solute breakthrough curve with exact solution of Advection Dispersion Equation (Ogata and Banks, 1961) using least-squares method and by considering hydrodynamic dispersion as a tuning parameter to determine the equivalent hydrodynamic dispersion.



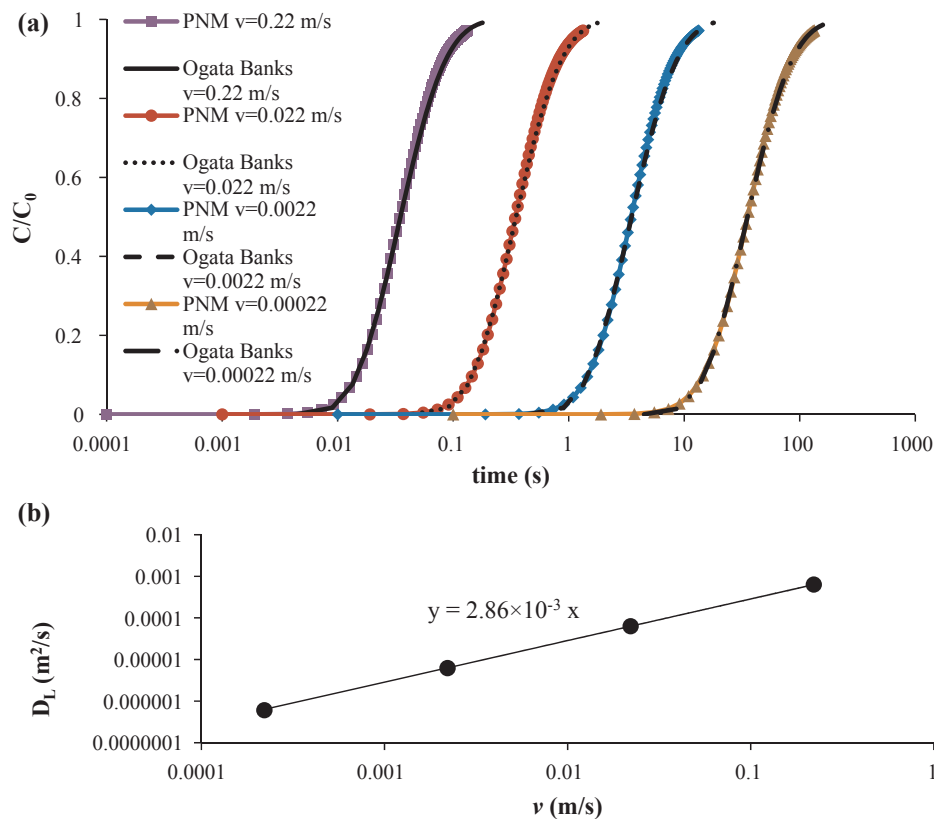


Fig. C.3. (a) Breakthrough curves obtained through pore network simulation and by Ogata-Banks exact solution for the pore network at 2 cm peat depth profile; (b) Variation of hydrodynamic dispersion with average linear flow velocity for the PNM of peat at 2 cm depth.

For PNMs of peat soil, simulating the solute breakthrough curve and fitting it with exact solution are repeated four times in different water velocities (e.g. 0.00022, 0.0022, 0.022, and  $0.22 \text{ m.s}^{-1}$  in Fig. C.3a), giving the variation of hydrodynamic dispersion with average linear flow velocity. Then, the dispersivity of each PNM is calculated as the slope of  $D_L$  vs.  $v$  data (e.g. 2.86 mm in Fig. C.3b).

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